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(71) Applicant: **EXXON RESEARCH AND
ENGINEERING COMPANY**
P.O.Box 390, 180 Park Avenue
Florham Park, New Jersey 07932 (US)

(72) Inventor: **Saleh, Ramzi Yanni**
13, Fir Court
Flemington, New Jersey (US)
Inventor: **Wellman, William Edward**
10, Wayne Court
Edison, New Jersey (US)

(74) Representative: **Fletcher Watts, Susan J. et al**
Esso Engineering (Europe) Limited., Patents
and Licenses, Mallpoint 72, Esso House,
Ermyn Way
Leatherhead, Surrey KT22 8XE (GB)

(84) **Process for separation of hydrolyzable polymers from non-hydrolyzable polymers.**

(87) The present invention relates to a process for reactively separating hydrolyzable polymers, such as PET, in mixtures of the polymer and certain non-hydrolyzable polymers, specifically polyolefins by converting the hydrolyzable polymers to their corresponding water soluble components (e.g., PET to ethylene glycol and terephthalic acid) in the presence of liquid water at temperatures from about 200°C up to the critical temperature of water and autogenous pressure. The process has utility in recycling and waste material separation processes.

The process of the present invention constitutes a means for the reactive separation of hydrolyzable polymers such as polyethylene terephthalate resins ("PET"), polyamides, polycarbonates, polyethers, polyacrylonitriles in mixtures with polyolefins such as polypropylene ("PP") and polyethylene ("PE") by selectively converting the hydrolyzable polymers to their starting materials, e.g., PET to terephthalic acid ("TPA") and ethylene glycol ("EG").

The hydrolysis of high molecular weight condensation polymers such as PET in the absence of added acids or bases, is well known in the art. When, for example the condensation polymer is PET, the primary hydrolysis products are TPA and EG, see, e.g., U.S. Patent No. 4,578,510, U.S. Patent 4,805,762, U.S. Patent 4,620,032 and U.S. Patent No. 3,120,581. However, the art does not teach nor suggest a process for the reactive separation of condensation polymers such as PET, polyamides, polycarbonates, polyethers, polyvinylchlorides, and polyacrylonitriles from mixtures containing other polymer resins by hydrolyzing the condensation polymer into its water-soluble components in the presence of neutral liquid water as a starting material in the absence of any externally supplied acids or bases and at autogenous pressure.

This invention provides a process for the reactive separation of hydrolyzable polymers, such as PET, polyamides, polycarbonates, polyethers, polyvinylchlorides, and polyacrylonitriles in mixtures with non-hydrolyzable polyolefins such as PP and PE by selectively converting PET to TPA and EG by contacting the mixture with neutral liquid water as a starting material (pH equals 7.0) at a temperature of at least 200°C, preferably from about 200°C to about 350°C, more preferably from about 225°C to about 325°C, at the pressure generated by the mixed components of the system at the corresponding temperature ("autogenous pressure"). The products resulting from the conversion of the products remain in the hot liquid water phase and may be separated.

All materials used herein may be obtained from commercial sources.

The hydrolyzable polymers are preferably PET, polyamides, polycarbonates, polyethers, and polyacrylonitriles polymers in mixtures with non-hydrolyzable polymers, preferably polyolefins such as PP, PE alone or in mixtures thereof. As used herein, "hydrolyzable" refers to decomposition of the C-O bonds in the backbone of a polymer by hydrolysis under the conditions of the present invention.

In the starting mixture, the hydrolyzable and non-hydrolyzable polymers may be present in any form that can be accommodated by the reaction vessel, thus powders crystals, small chips are acceptable. The selective reactive separation of the PET, polyamides, polycarbonates, polyethers, and polyacrylonitriles (collectively referred to herein as "hydrolyzable polymers") in a mixture of th hydrolyzabl poly-

mers and non-hydrolyzable polymers, specifically polyolefins such as PP and PE, is carried out by contacting the starting materials of the non-hydrolyzable and hydrolyzable polymers and neutral liquid water at a temperature of preferably from about 200°C up to the critical temperature of water, which is about 374°C, preferably from about 200°C to about 350°C, more preferably from about 225°C to about 325°C for a time sufficient to convert the hydrolyzable polymer(s) to corresponding water soluble components. The identity of such components are well known to one ordinarily skilled in the art. Polyolefins in the mixture are not hydrolyzable polymers at the reaction conditions of the process of the present invention.

The time period for which the starting materials are contacted is not generally critical provided it is a sufficient time to allow the hydrolyzable polymers to convert to their water soluble components. This period may be, for example, from half an hour to a few days or more, but is usually from half an hour to six hours.

The amount by weight of water to polymer is generally from about 1:1 - 20:1, preferably from about 2:1 - 10:1. The reaction is carried out at autogenous pressure (i.e., vapor) the pressure generated by the mixed components system at the given reaction temperature which typically, for liquid water alone will be from about 225.45 psi at 200°C to about 2397.79 psi at 350°C. It is within the skill of one ordinarily skilled in the art to determine such pressures, and the pressure of liquid water in the above temperature range may be determined by reference to standard tests. See, e.g., CRC Handbook of Chemistry and Physics, 61st Edition, p. D-197 (1980-1981).

In the process of the present invention, liquid water, the hydrolyzable polymers, and the non-hydrolyzable polymers are preferably the only starting materials. The products resulting from contacting the starting materials of the polymers and neutral liquid water under the reaction conditions of the present invention are such that the hydrolyzable polymers produce products that are soluble in hot water and, thus, remain in the hot liquid water phase, while the non-hydrolyzable polymers (polyolefins) form a separate, solid phase. The two phases may be separated by any means known to one skilled in the art, for example, by filtration, by such contact and thus are present as a separate, solid phase. For example, when the starting mixture contains PET, PE and PP, and neutral liquid water the contacting reactively separates the PET by producing TPA and EG that remain in the aqueous layer; the PP and PE are not hydrolyzed by such contacting. The products of PET hydrolysis, TPA and EG, are recoverable from the hot liquid water phase layer.

The process has utility in plastics recycling by providing a simple method for differentiating by reactive separation hydrolyzable polymers from which

starting materials can be recovered from other non-hydrolyzable polymers (polyolefins) which then can be used in conversion processes, and has utility as a method for reactive purification of non-hydrolyzable polymers (polyolefins) so that they can be used in other conversion processes.

The process of the present invention may be understood by reference to the following examples.

Example 1

A mixture of PET (plastic soda containers), polyamides (nylon), and polycarbonates was cut into small pieces and placed in a minibomb with an approximately five-fold excess by weight of water to the total amount by weight of polymer. The temperature was raised to approximately 315°C for 2 hours. At the end of the 2-hour period, the hot liquid phase containing the hydrolysis products, terephthalic acid and ethylene glycol, was separated from the solid phase which contained the polyolefins.

Example 2

The procedures of Example 1 were repeated, except that the temperature was raised to 350°C. As in example 1, this temperature was maintained for 2 hours. At the end of the 2-hour period, the hot liquid water phase containing the hydrolysis products, terephthalic acid and ethylene glycol, was separated from the solid phase which contained the polyolefins.

Claims

1. A process for the reactive separation of certain hydrolyzable polymers from certain non-hydrolyzable polymers in mixtures thereof by selectively converting said hydrolyzable polymers to their water soluble components comprising:

(a) contacting the starting materials of neutral liquid water and a mixture of hydrolyzable polymers selected from PET, polyamides, polycarbonates, polyethers, polyacrylonitriles, and non-hydrolyzable polymers selected from polyolefins;

(b) heating the starting materials to a temperature of from about 200°C up to critical temperatures of water to autogenous pressure for a time sufficient to convert the hydrolyzable polymer to corresponding water soluble components.

2. The process of claim 1 wherein the polyolefins are selected from polypropylene and polyethylene and mixtures thereof.

3. The process of claim 1 or 2 wherein the temper-

ature is from about 200°C to about 350°C.

4. The process of claim 1 or 2 wherein the temperature is from about 225°C to about 325°C.

5. The process of any preceding claim further comprising separating the water soluble components from the non-hydrolyzable polymers.